

**IN THE CLAIMS:**

Amend Claims 91, 97, 98, 100-107, 109 and 110 as follow:

Claims 1-90. Canceled

91. (Currently Amended) Zeolite N having a composition according to the formula

$(M_{1-a}, P_a)_{12}(Al_bSi_c)_{10}O_{40}(X_{1-d}, Y_d)_2 nH_2O$  where

M = alkali metal or ammonium;

P = alkali metal, ammonium or metal cations exchanged in lieu of alkali metal or ammonium

X = halide and Y is an anion and

$0 \leq a \leq 1$ ,  $1 \leq c/b \leq \infty$ ,  $0 \leq d \leq 1$  and  $1 \leq n \leq 10$

with the proviso that when  $a = 0$ ,  $b = 1$ ,  $c = 1$ ,  $d = 0$  and  $X = Cl$ , then M  $\neq$  K (potassium).

92. (Previously Presented) Zeolite N as claimed in claim 91, having a BET surface area greater than  $1 m^2/g$ .

93. (Previously Presented) Zeolite N as claimed in claim 92 having a BET surface area between  $1 m^2/g$  and  $150 m^2/g$ .

94. (Previously Presented) Zeolite N having a structure as claimed in claim 92 having a proportion of external surface area to internal surface area of greater than 1%.

95. (Previously Presented) Zeolite N as claimed in claim 94 having a proportion of external surface area to internal surface area of greater than 5%.

96. (Previously Presented) Zeolite N as claimed in claim 91 having an X-ray diffraction pattern which has a high background intensity of greater than 5% of a maximum peak height between the region  $25^\circ < 2\theta < 70^\circ$ .

97. (Currently Amended) A method of exchanging ammonium ions in solution including the step of contacting a zeolite Zeolite N as claimed in claim 91 with a solution ~~when used for exchange of ammonium ions in solution.~~

98. (Currently Amended) The method of claim 97 wherein the exchange of ammonium ions in solution is carried out ~~Zeolite N as claimed in claim 91 when used for exchange of ammonium ions~~ in the presence of alkali metal and/or alkaline earth metal ions ~~in solution.~~

99. (Previously Presented) Zeolite N as claimed in claim 91 having a cation exchange capacity ranging from 100 meq per 100g to 700 meq per 100g for ammonium ions with concentrations between less than 1 mg/L to greater than 10, 000 mg/L.

100. (Currently Amended) A method of exchanging metal ions in solution including the step of contacting a zeolite Zeolite N as claimed in claim 91 with a solution ~~when used for exchange of metal ions in solution.~~

101. (Currently Amended) The method of claim 100 wherein the exchange of metal ions in solution is carried out ~~Zeolite N as claimed in claim 91 when used for exchange of metal ions~~ in the presence of alkali metal or alkaline earth metal ions ~~in solution.~~

102. (Currently Amended) A method of adsorbing ammonia gas including the step of contacting a zeolite Zeolite N as claimed in claim 91 with ~~when used for adsorbing ammonia gas~~ in the temperature range 0°C to 300°C.

103. (Currently Amended) The method of claim 102 wherein the adsorption of ammonia gas is carried out ~~Zeolite N as claimed in claim 91 when used for adsorbing ammonia gas~~ in the temperature range 0°C to 300°C in the presence of water.

104. (Currently Amended) A method of absorbing oil including the step of contacting a zeolite Zeolite N as claimed in claim 91 ~~with the~~ when used for absorbing oil.

105. (Currently Amended) The method of claim 104 wherein the zeolite Zeolite N absorbs as claimed in claim 104 ~~when used for absorbing oil~~ greater than 50g of oil per 100g of zeolite Zeolite N.

106. (Currently Amended) A method of removing anions from wastewater including the step of contacting a zeolite Zeolite N as claimed in claim 91 ~~with~~ when used for removing anions within from wastewater.

107. (Currently Amended) A method of re-exchanging alkali metal ions from a solution containing hydroxyl ions including the step of contacting an ammonium form of a zeolite Zeolite N as claimed in claim 91 ~~with~~ when used in an ammonium form to have a capacity to re-exchange alkali metal ions within a solution ~~from solutions~~ containing hydroxyl ions ranging in concentration from 0.1 M to 2.0 M.

108. (Previously Presented) Zeolite N as claimed in claim 91 having a removal rate of ammonium ion ranging between 50-100% from ammonium loaded Zeolite N using a regeneration solution containing hydroxyl ions.

109. (Currently Amended) A method of re-exchanging ammonium ions and/or of retaining a high selectivity for ammonium ions in a zeolite N including the step of contacting a Zeolite N as claimed in claim 91 ~~with the~~ when used to re-exchange ammonium ions and/or to retain high selectivity for ammonium ions after regeneration of the zeolite N with a solution containing hydroxyl ions.

110. (Currently Amended) A method of killing gram positive or gram negative bacteria including the step of contacting a zeolite Zeolite N as claimed in claim 91 with the ~~when used to kill~~ gram positive or gram negative bacteria.

111. (Previously Presented) Zeolite N as claimed in claim 91 where c/b is greater than 1.

112. (Previously Presented) Zeolite N as claimed in claim 111 where c/b has an upper value of 3.

113. (Previously Presented) Zeolite N as claimed in claim 111 where c/b has an upper value of 5.

114. (Previously Presented) Zeolite N as claimed in claim 91 where Y is hydroxyl or halide.

115. (Previously Presented) Zeolite N as claimed in claim 114 where Y is chloride.